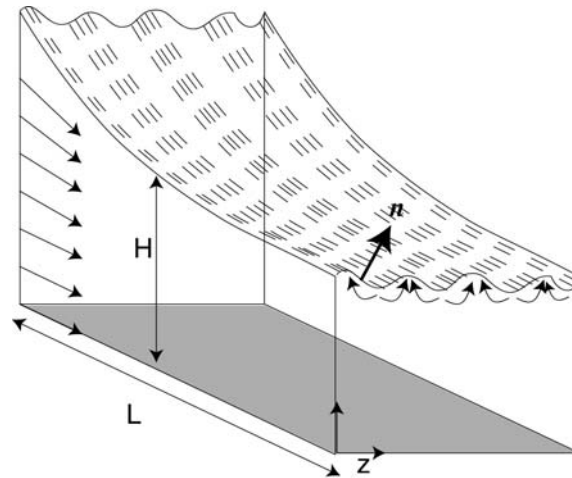


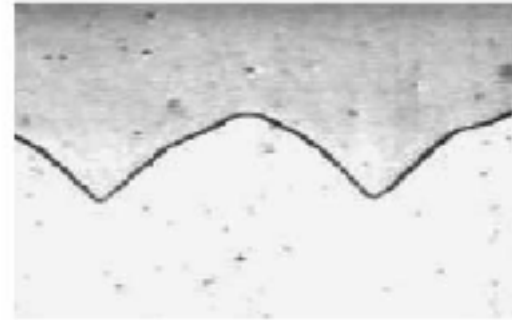
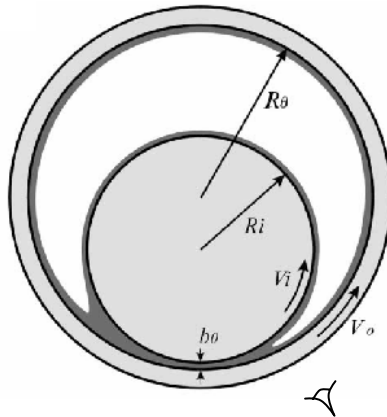
Interfacial hoop stress and viscoelastic free surface flow instability



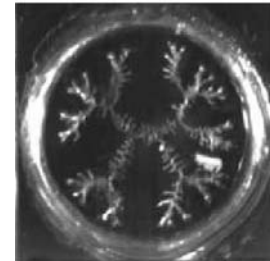
Michael D. Graham
University of Wisconsin-Madison

Free surface instabilities of viscoelastic flows

Eccentric cylinders
(Varela-Lopez
et al 2002)



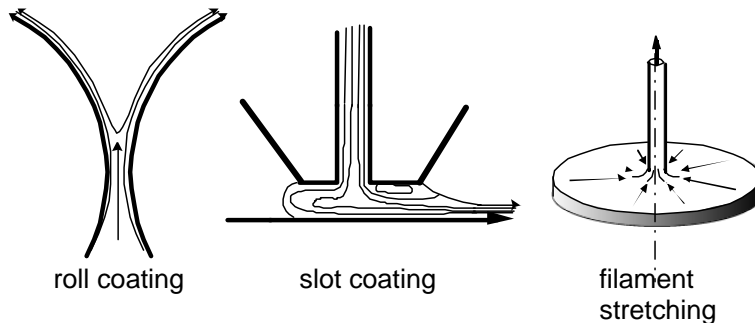
Filament stretching
(Sridhar &
McKinley 2002)



G .H. McKinley

- Viscoelasticity dramatically exacerbates many free surface instabilities

Viscoelastic free surface flows: theory and computation



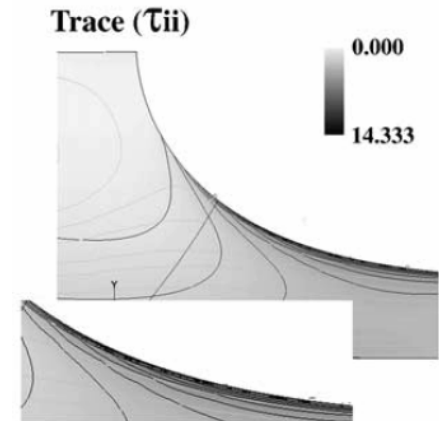
Weissenberg number

$$Wi = \lambda \dot{\gamma}$$

λ relaxation time

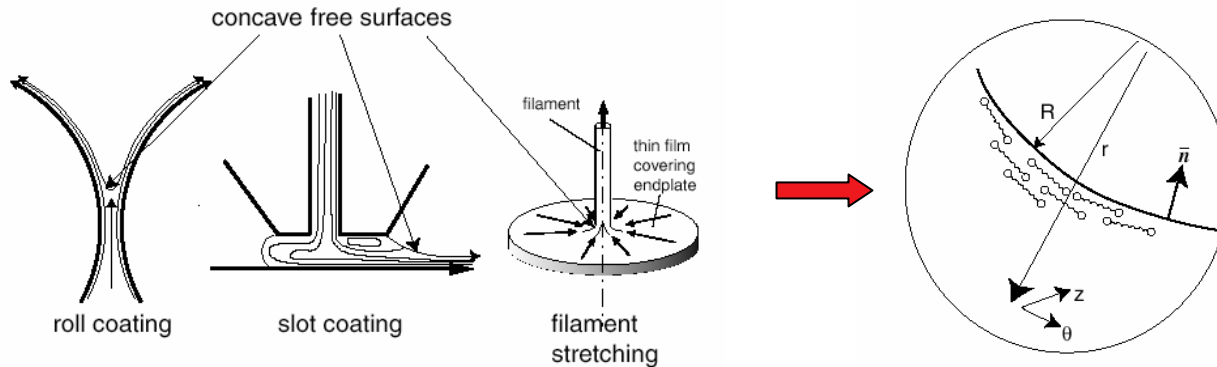
$\dot{\gamma}$ strain rate

- Lubrication approximation: tractable formulation at high Wi that keeps dominant viscoelastic effects has not been worked out
- Low Wi asymptotic analysis (Ro and Homsy 1995): effects of viscoelasticity are small
- CFD approaches (Scriven, Khomami, Pasquali)
 - can predict film thickening when $Wi=O(1)$
 - challenging: thin stress b.l.s arise at free surfaces
 - linear stability analysis at high Wi has not been performed
- Present work: simple models that incorporate key physical effects



Polymer stress in Hele-Shaw coating (Lee *et al.* 2002)

Stress at a concave free surface



Approximate local free surface shape as an arc, neglect gravity for clarity: normal stress balance for a 2D flow yields:

$$\begin{aligned} \frac{\partial \bar{\sigma}_{rr}}{\partial r} &= \frac{\bar{\sigma}_{\theta\theta} - \bar{\sigma}_{rr}}{R} \\ &\equiv \frac{\Delta\sigma}{R} \\ &\equiv T \end{aligned}$$

For **Newtonian** fluids, T can be estimated from the bulk pressure gradient

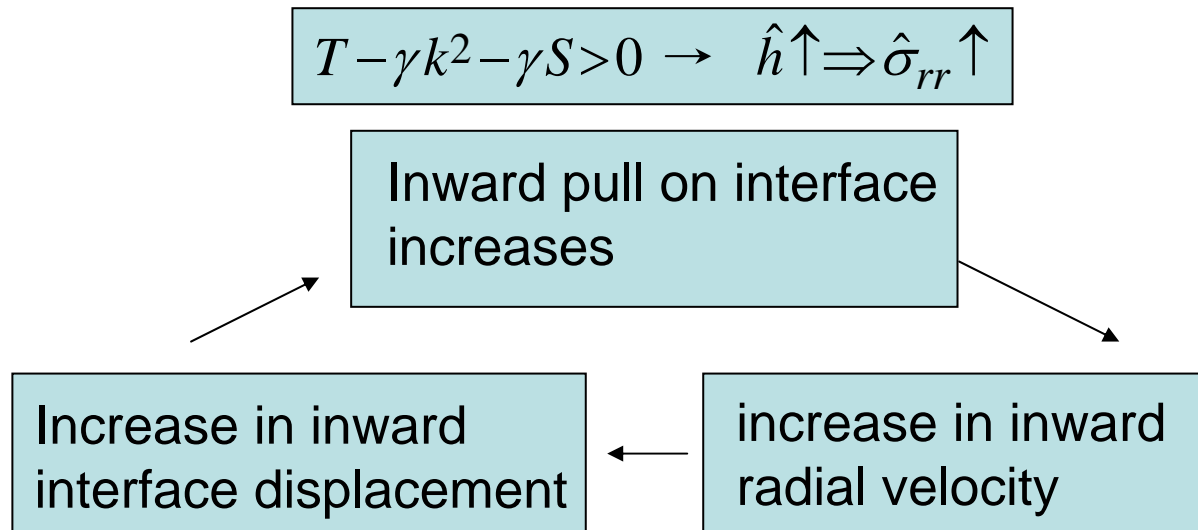
Perturbation normal stress balance

Let radial position of surface be

$$r = \bar{h} - \hat{h}(\theta, t)e^{ikz}$$

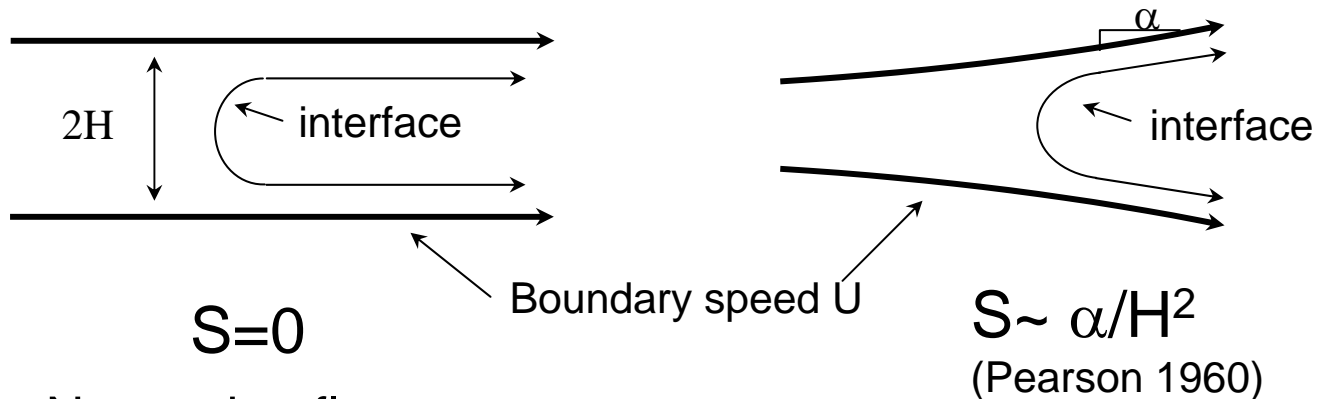
Normal stress balance becomes:

$$\begin{aligned} \hat{\sigma}_{rr} \Big|_{r=\bar{h}} &= T\hat{h} + \gamma \left(-k^2 + \frac{1}{R^2} \frac{\partial^2}{\partial \theta^2} + \frac{1}{R^2} \right) \hat{h} \\ &\approx (T - \gamma k^2 - \gamma S) \hat{h} \end{aligned}$$



$T = \Delta\sigma/R = \text{hoop stress} * \text{curvature} = \text{general driving force for free surface flow instability}$

Newtonian Hele-Shaw and roll-coating flows



Newtonian flow:

- $\Delta\sigma \sim \eta U/H$ (bulk stress \sim interfacial stress \sim viscous stress)
- $R \sim H$
- $T = \Delta\sigma / R \sim \eta U/H^2$

Newtonian instability criterion becomes

$$Ca = \eta U / \gamma \sim \alpha + (kH)^2 \leftarrow \text{Incorrect exponent comes from local approx.}$$

(Saffman & Taylor, Pearson, Pitts & Greiller...)

Effect of viscoelasticity

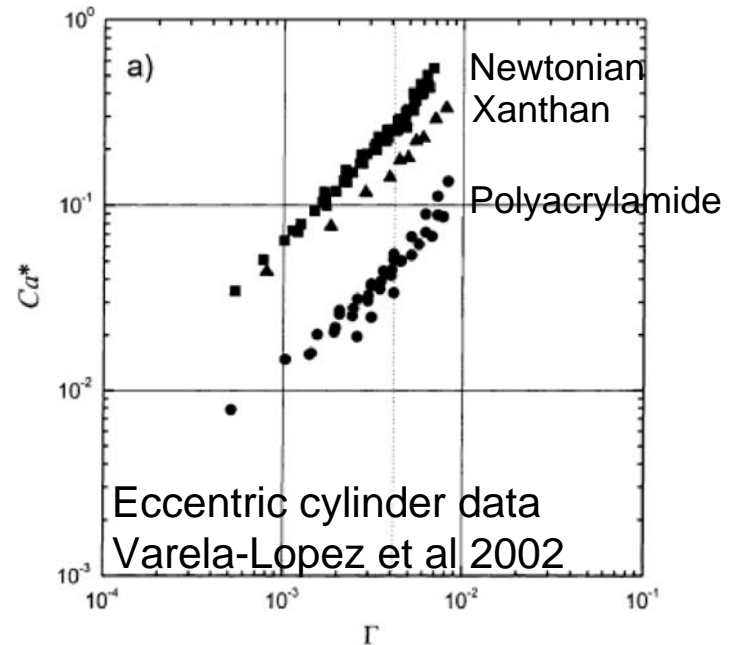
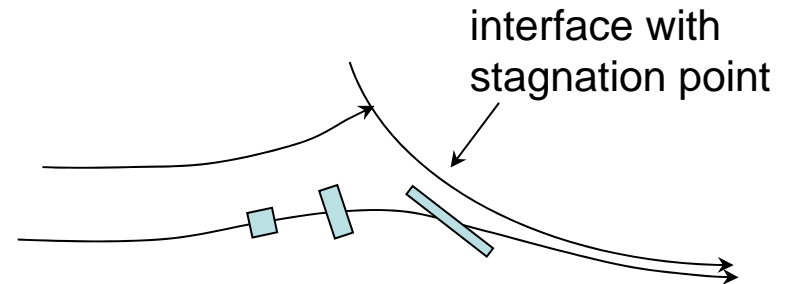
Is the bulk stress a good estimate of the interfacial stress?

No.

- Flow near a free surface is always extensional
 - **strain \sim (distance from free surface) $^{-1}$**
- \Rightarrow stress boundary layers
 \Rightarrow We should estimate $\Delta\sigma$ with an extensional viscosity η_e : $\eta_e \gg \eta$

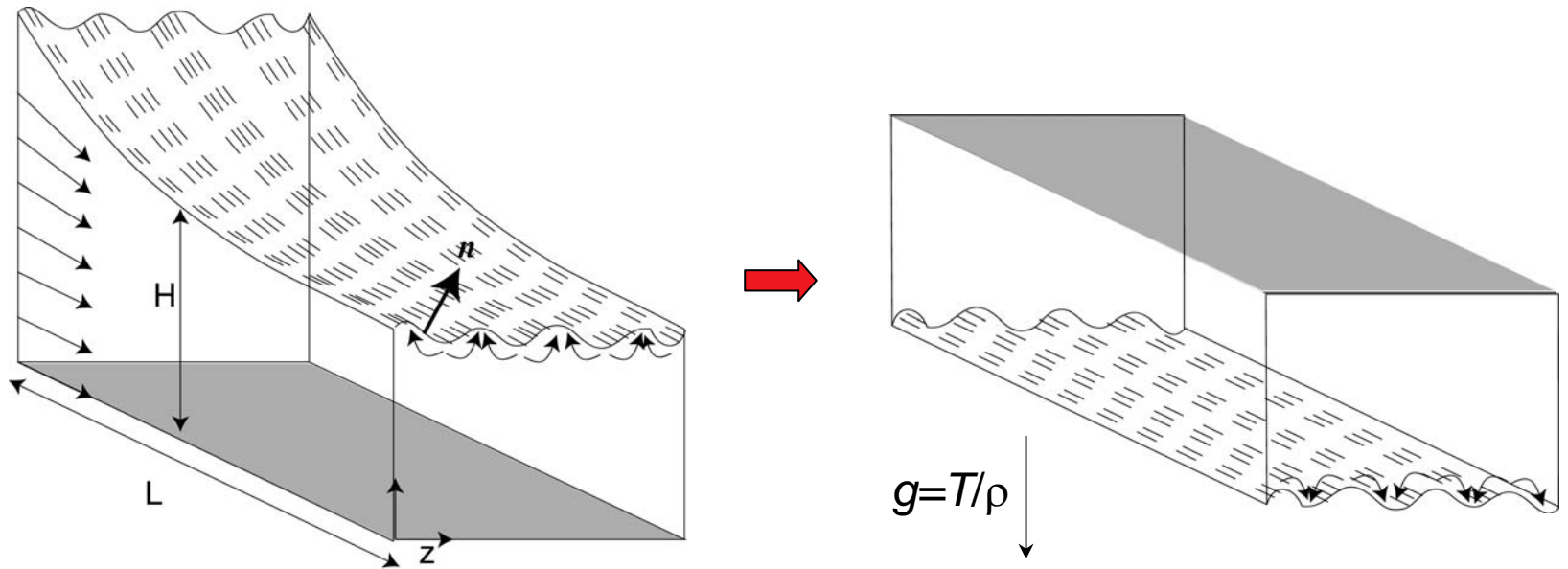
\Rightarrow Modified instability criterion

$$Ca \eta_e / \eta \sim \alpha + (kH)^2$$



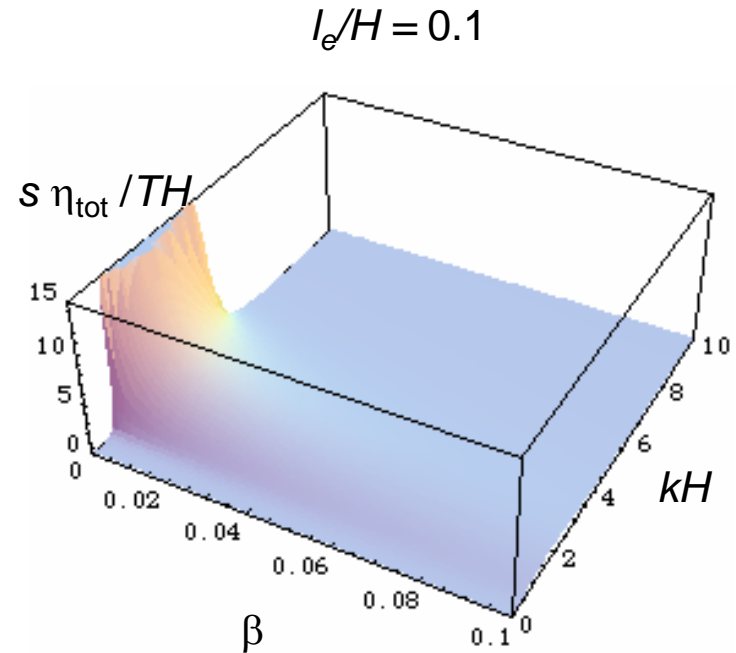
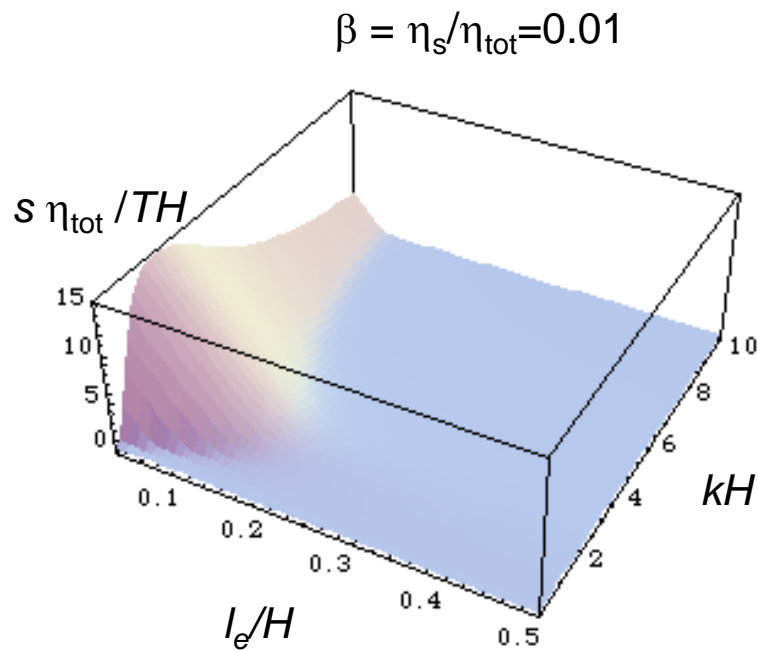
Viscoelastic free surface instability

a solvable special case



- $H \ll L, R = L$
 - Let curvature $K=H/R \rightarrow 0$ with $K\Delta\sigma$ finite.
 \Rightarrow viscoelastic Rayleigh-Taylor problem (cf. Aitken & Wilson 1993), but with ρg replaced by T
- New intrinsic elastic length scale $l_e = G/T$, where G is shear modulus

Results for inertialess Oldroyd-B model, $\gamma=0$



- Maximum growth rate s is at $kH = 2.2$
- Newtonian: $s \eta_{\text{tot}} / TH < 0.16$ for all k
- Viscoelastic: $s \eta_{\text{tot}} / TH \sim \beta^{-1}$ for $I_e < 0.16H$; **why the blowup?**

Energy integral scalings

$$kH \gtrsim 1$$

$K =$ kinetic energy: $\frac{\rho}{k^2} s^3$

$E =$ strain energy: Gs

$W =$ work done by the surface perturbation: $\frac{T}{k} s$

$D =$ dissipation: $\eta_s s^2$

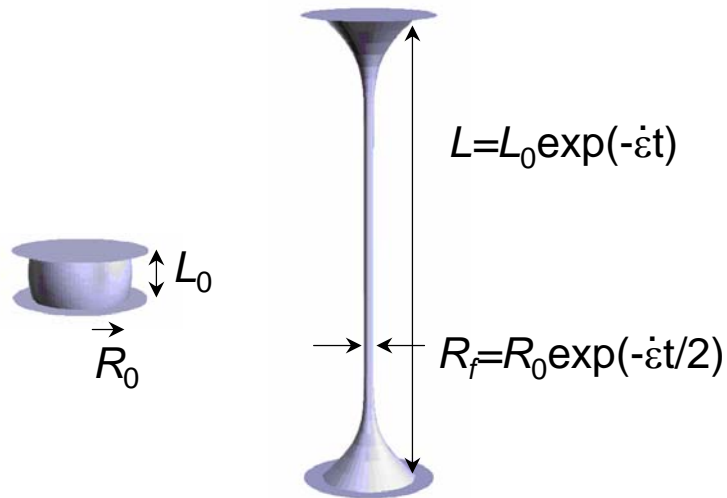
$$K+E+D=W$$

$$W \gg E \text{ for } T \gg Gk \text{ (} kl_e \ll 1 \text{)}$$

- l_e : length scale where surface work and strain energy balance
 \Rightarrow For small l_e , surface work must be balanced by inertia or solvent viscosity
-- strain energy can't keep up
 \Rightarrow s blows up for small ρ and η_s

Filament stretching rheometer

Schematic



Instability near endplates
(McKinley & coworkers)



side view

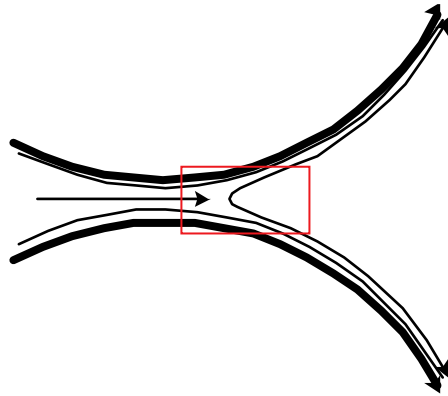
bottom view

- Extensional rheology of polymer solutions
- Simulations show stress boundary layers near free surface

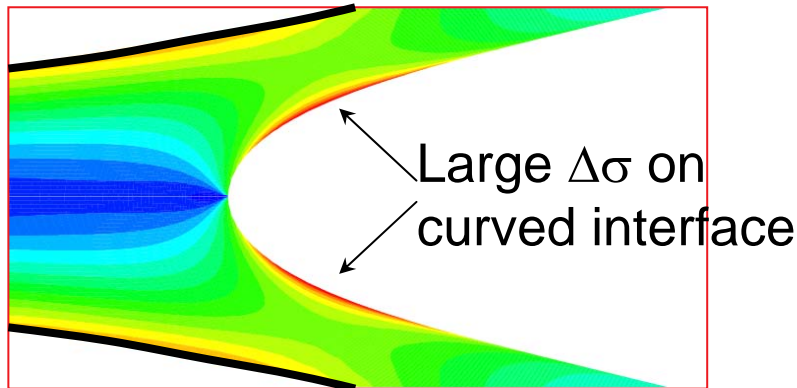
Roll coating: computational results

(courtesy of M. Pasquali)

geometry

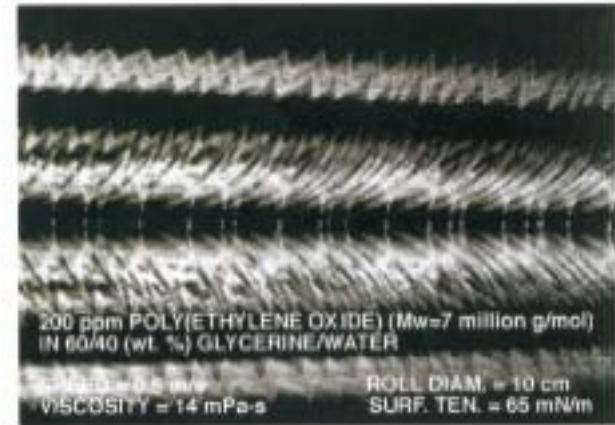


σ_{tt} in meniscus region



- Steady state viscoelastic computations, FENE-P model
- Stress boundary layers form
- $\Delta\sigma$ greatly exceeds Newtonian value

Instability in VE roll coating



$Ca=2.0$, $We=2.0$, FENE-P, $b=50$, $\beta=0.59$

Carvalho et al. 1994

Instability prediction for filament stretching

Estimates:

$$\frac{\Delta\sigma}{R} > k^2\gamma$$

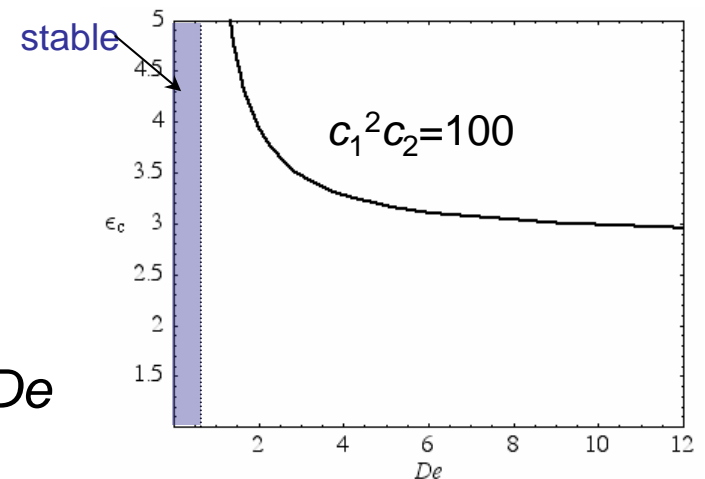
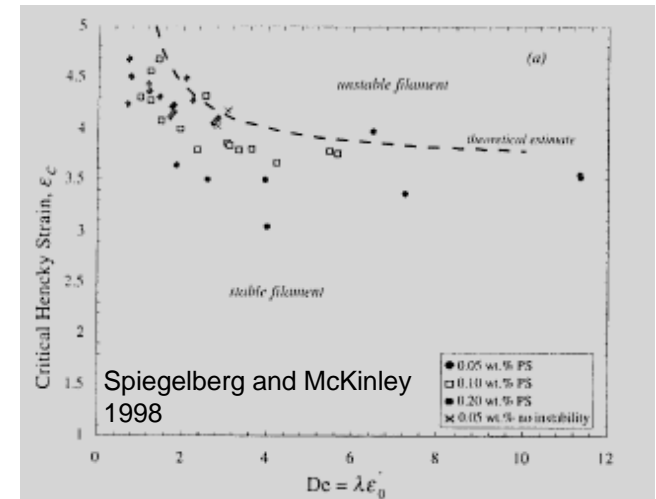
- $\Delta\sigma$: Oldroyd-B, uniaxial extension
- wavenumber $k = c_1/R_f$, $c_1 = O(1)$
- radius of curvature $R = c_2 R_f$, $c_2 = O(1)$
- $\gamma/GR_0 = 0.69$

Predicted critical strain:

$$\varepsilon_c = \left(\frac{3}{2} - \frac{1}{De} \right)^{-1} \log \left(\frac{c_1^2 c_2 \gamma}{GR_0} \left(1 - \frac{1}{2De} \right) \right)$$

⇒ Stable region captured well

⇒ Overall trend reasonable until high De

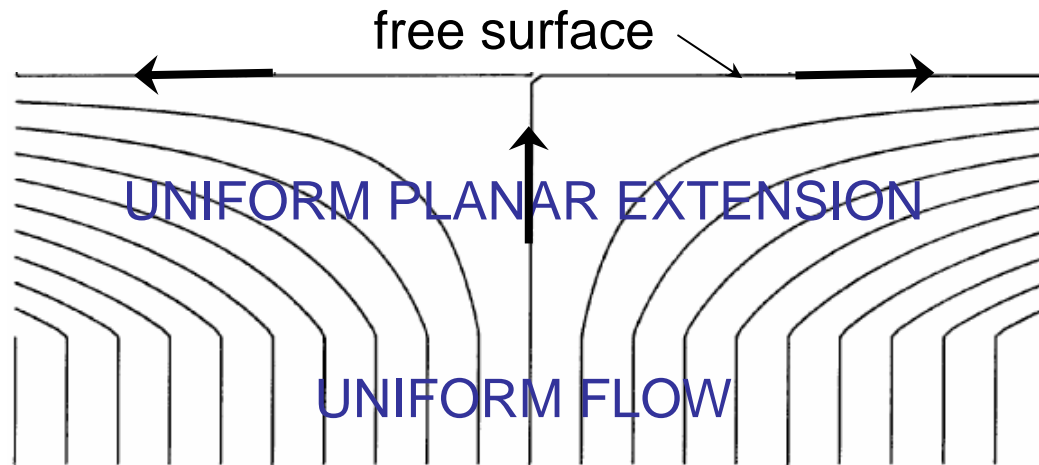


Conclusions

- Interface tension * curvature drives free surface flow instabilities:
 - ⇒ generalized Saffman-Taylor result
 - ⇒ connection to bulk viscoelastic instabilities
- A special case can be explored in detail by reduction to viscoelastic Rayleigh-Taylor instability
- Elasticity introduces a new length scale
- Growth rates can be large: surface work overcomes strain energy
- Application of simple theory to filament stretching gives good agreement with $O(1)$ free parameters

Thanks: G. M. Homsy, KITP (UC-Santa Barbara),
NSF, ACS/PRF

Stress boundary layers in viscoelastic free surface flows: a model flow



- Stress is independent of x
- Stress increases exponentially toward free surface for $Wi > 1/2$.

