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*DYNAMICS OF SUSPENDED  
COLLOIDAL PARTICLES  
NEAR A WALL*

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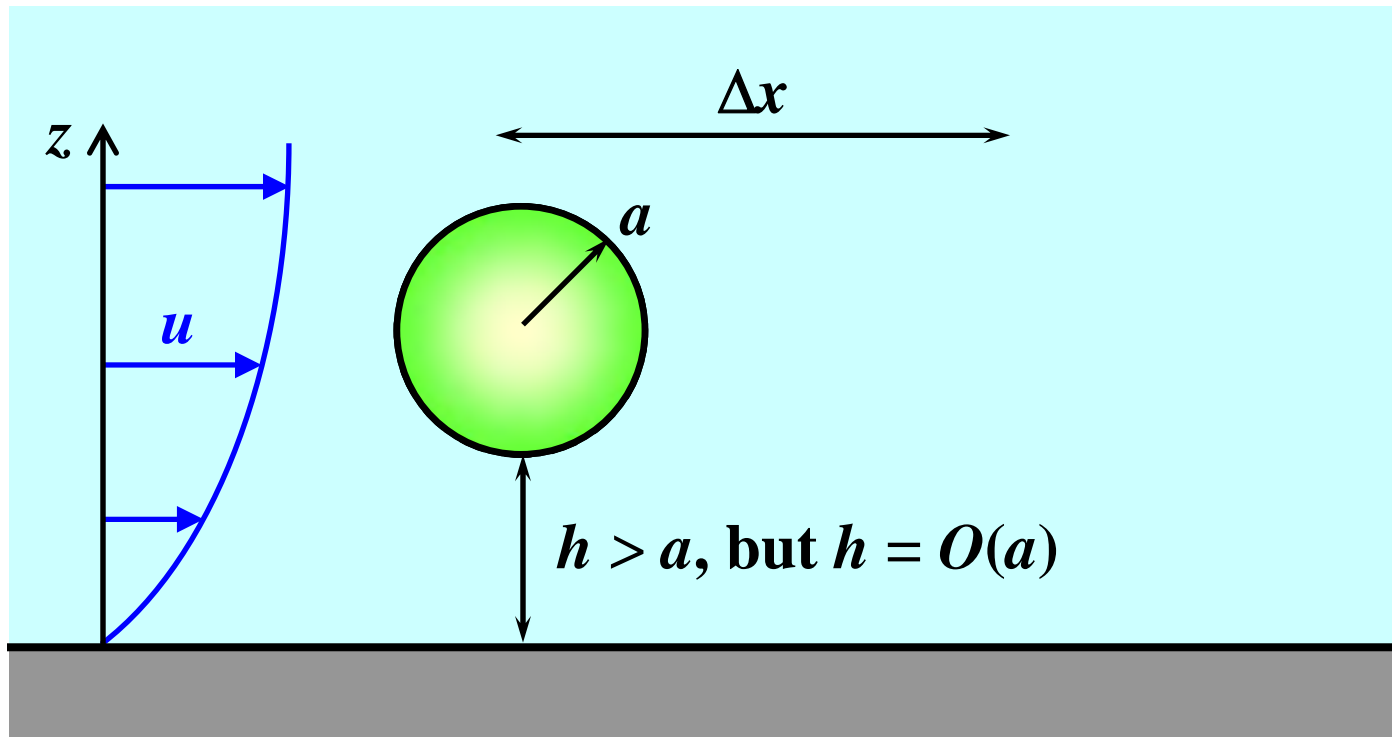
# *OUTLINE*

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- **The problem and its motivation**
- **The (evanescent-wave PTV) technique**
  - Near-wall particle distributions and displacements
- **Poiseuille flows**
- **Electrokinetically driven flows**
- **Summary**

# A PARTICLE NEAR A WALL

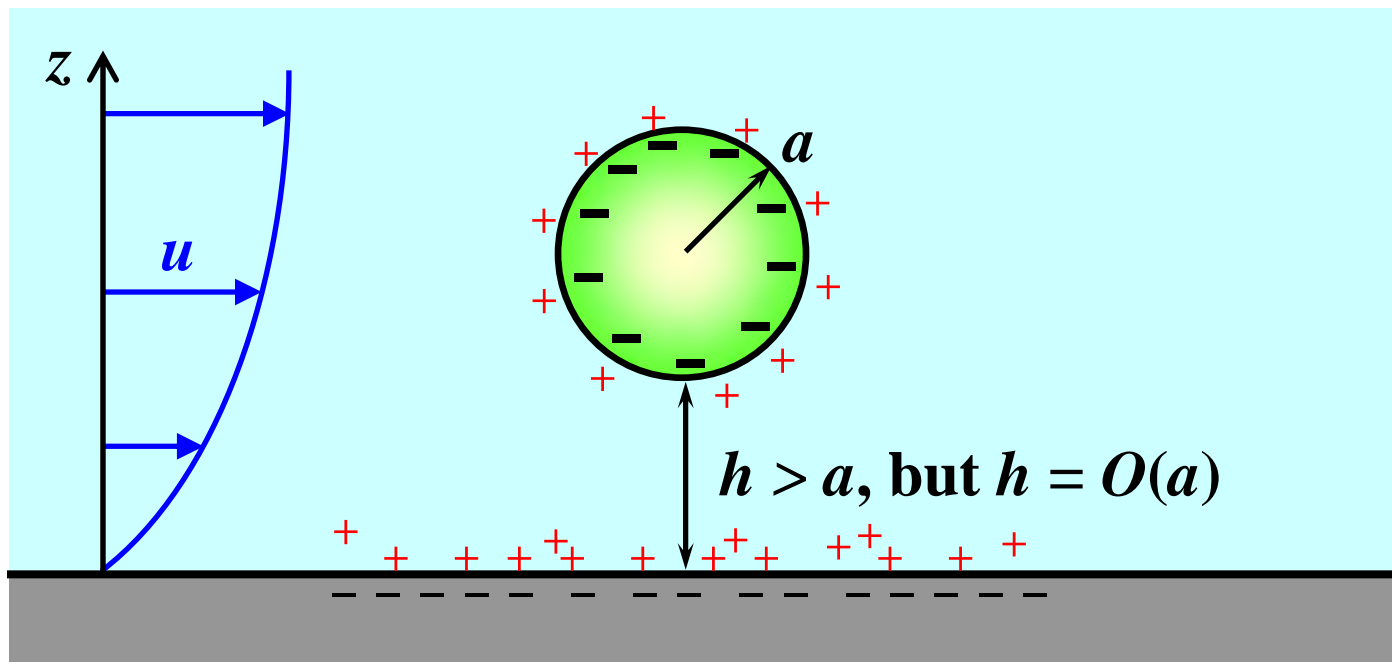
- **What are the dynamics of a particle suspended in a flowing fluid near a solid wall?**
  - How is the particle velocity related to the fluid velocity?



# A PARTICLE NEAR A WALL

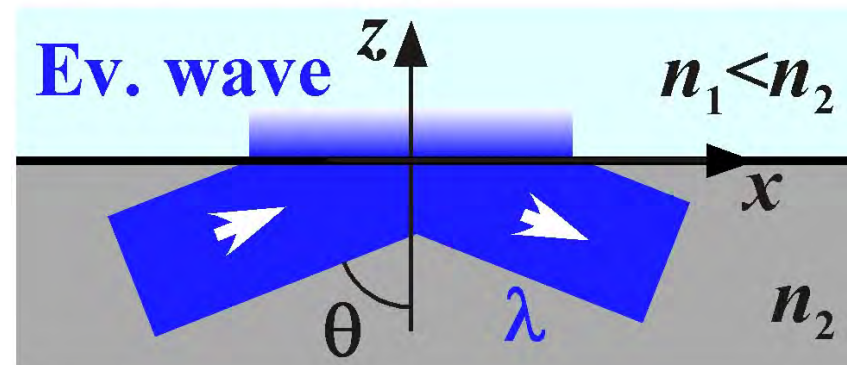
## ■ Another complication

- Wall, particle surfaces charged
- Fluid conducting with mobile ions: electric double layers (EDL) on particle, wall surfaces

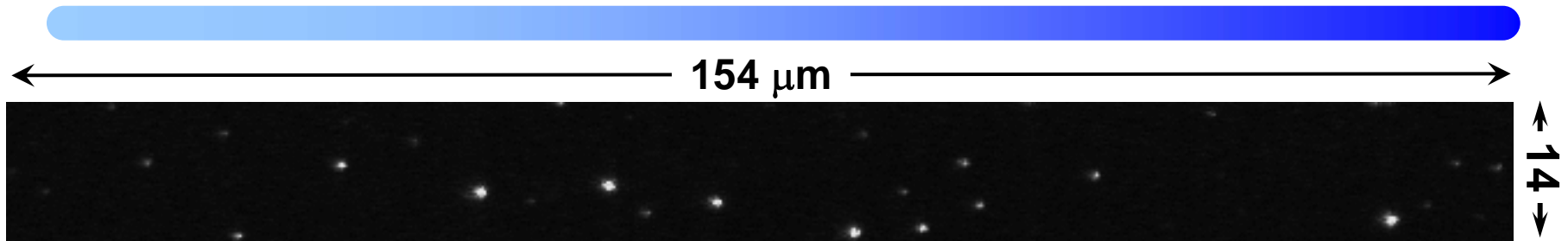


# INTERFACIAL TRANSPORT

- **Microfluidics: flows with length scales of  $O(1-10^2 \mu\text{m})$** 
  - Faster diffusion:  $\tau_D \propto (\delta_D)^2$
  - Large surface areas, small volumes  $\Rightarrow$  surface forces significant
- **Characterize transport within  $O(1 \mu\text{m})$  of the wall**
  - Track fluorescent particles ( $a = 50 \text{ nm} - 500 \text{ nm}$ ) illuminated by evanescent waves created at solid-fluid (refractive index) interface by total internal reflection of light
  - $I(z) = I_0 \exp \{-z / z_p\}$
  - $z_p = f(\lambda, \theta, n_1, n_2) \approx 100 \text{ nm}$  for glass-water interface
  - Image  $z \leq 4z_p$  based on imaging system noise floor



# EVANESCENT WAVE PTV



$a \approx 50 \text{ nm}$ ;  $\Delta t = 6 \text{ ms}$  (exp. 1 ms)

## ■ Brownian effects: $Pe = O(1-10^2)$

- Particle “mismatch”
- Asymmetric diffusion  $\Rightarrow$  overestimation of velocities

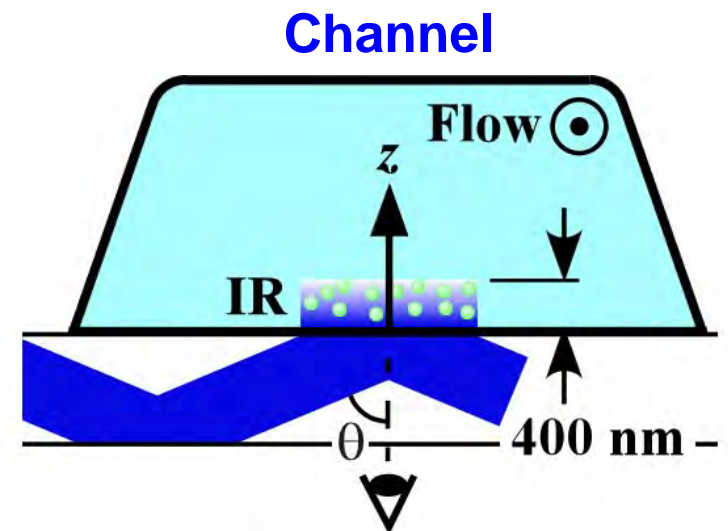
*Sadr et al. 07*

## ■ Nonuniform particle distribution

- EDL interactions, vd Waals effects
- Measure particle displacements and distributions

## ■ Nonuniform illumination

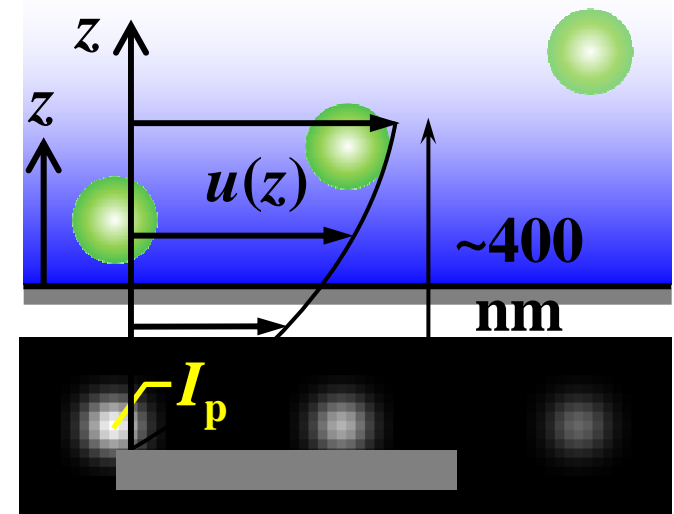
- Range of particle image sizes and intensities



# MULTILAYER PTV

## ■ Exploit nonuniform illumination to determine particle distributions and velocity profiles for $z < 400$ nm

- Assume particle image intensity  $I_p(z)$  has exponential decay with length scale  $z_p$  Li & Yoda 08
- Particle edge distance from wall  
$$h = z_p \ln\{I_p^0 / I_p\}$$



## ■ Steady-state particle distribution

- Variation in particle images ( $\sigma$  of  $I_p^0 = 9\%$ ), average over ensemble of  $O(10^5)$  particles

## ■ Near-wall (particle and fluid) velocity profile

- “Bin” particles into different layers based on  $h$ , then determine velocities parallel to wall at different  $z$  using particle tracking



*POISEUILLE FLOWS*





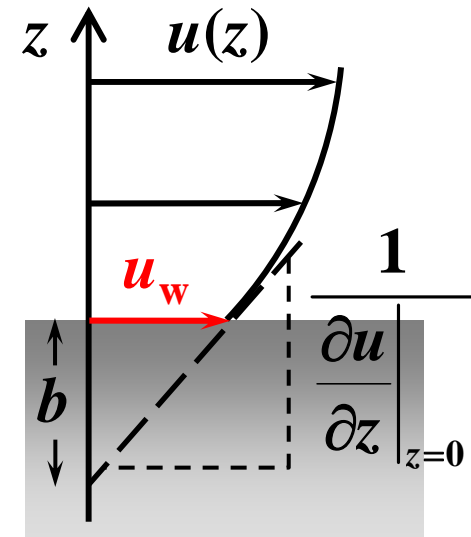
# SLIP

## ■ Is the no-slip boundary condition valid for $z < 1 \mu\text{m}$ ?

- Navier partial-slip BC:  
$$u_w = b \left. \frac{\partial u}{\partial z} \right|_{z=0}$$
$$b = \text{slip length}$$

## ■ Studies report $b \sim O(10\text{--}100 \text{ nm})$ for Newtonian liquids flowing over (mainly) nonwetting surfaces

- Local methods: slip lengths extrapolated from near-wall velocity data
- Wide variation in measured slip lengths
- Nonzero  $b$  attributed to surface wettability, (usually higher) shear rates, dissociated or gaseous layer (“nanobubbles”), change in fluid properties, ...



# POISEUILLE FLOW EXPTS.

- Study slip in fully-developed Poiseuille flow through  $H = 33 \mu\text{m}$  deep channel:  $Re_H = 0.03\text{--}0.12$

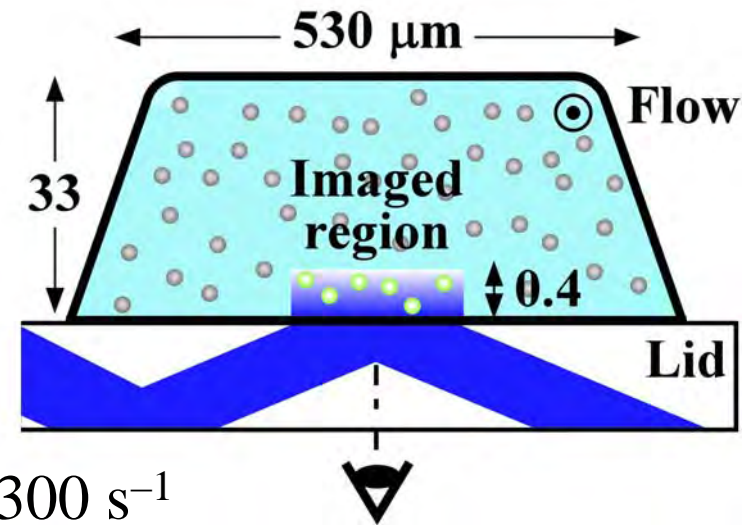
- Compare with exact solution

$$u(z) = \frac{H^2}{2\mu} \frac{\Delta p}{L} \left[ \frac{z}{H} \left( 1 - \frac{z}{H} \right) \right]$$

channel  $AR = 16$

- Linear velocity profile for

$$z < 400 \text{ nm: shear rate } \dot{\gamma} \approx 500\text{--}2300 \text{ s}^{-1}$$



- Hydrophobic, hydrophilic channels etched on same wafer

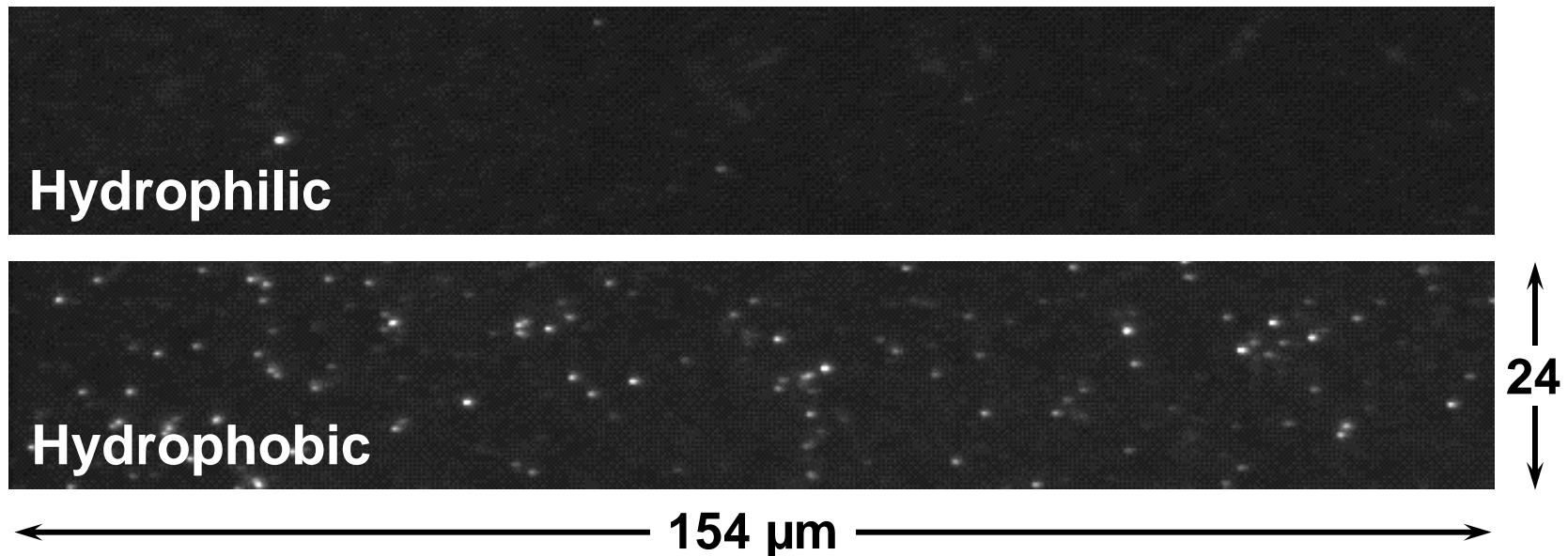
- Hydrophilic channels: untreated fused-silica walls with rms surface roughness  $\sim 3 \text{ nm} \Rightarrow$  contact angle  $28 \pm 4^\circ$
- Hydrophobic channels coated with  $\sim 2 \text{ nm}$  thick monolayer of OTS  $\Rightarrow$  contact angle  $100 \pm 4^\circ$

# EXPERIMENTAL DETAILS

## ■ Fluids

- Monovalent electrolyte solutions: different salt concentrations (2 and 10 mM), pH ( $\sim 6.4$  and  $\sim 7.7$ )
- Particles:  $a \approx 50$  nm fluorescent polystyrene;  $\phi \approx 20$  ppm
- Fluid with particles degassed for each experiment

## ■ Averaged “background” images (over 1200 images)



# PARTICLE DISTRIBUTIONS

- **Nonuniform distribution**

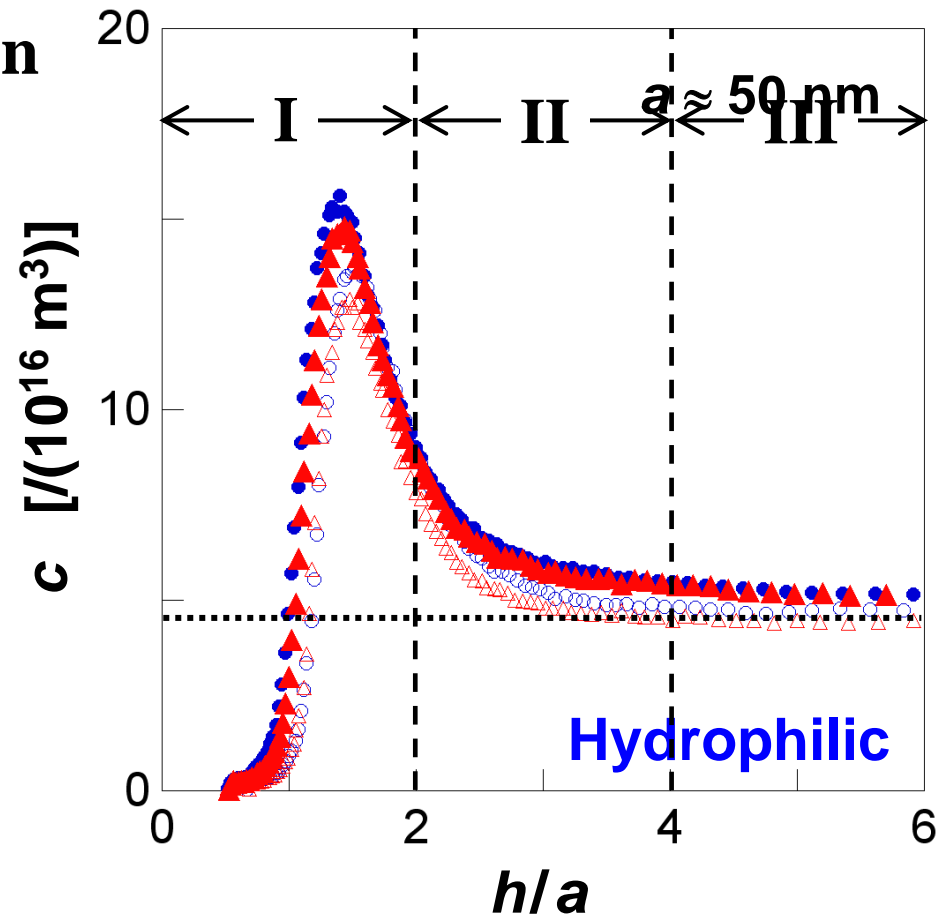
- Few particles at  $h/a < 1$
- Similar results for hydrophobic channel

- **“Bin” particles into 3 (sub)layers (particle center at  $z = h + a$ )**

- $1 \leq z_I / a \leq 3$
- $3 \leq z_{II} / a \leq 5$
- $5 \leq z_{III} / a \leq 7$

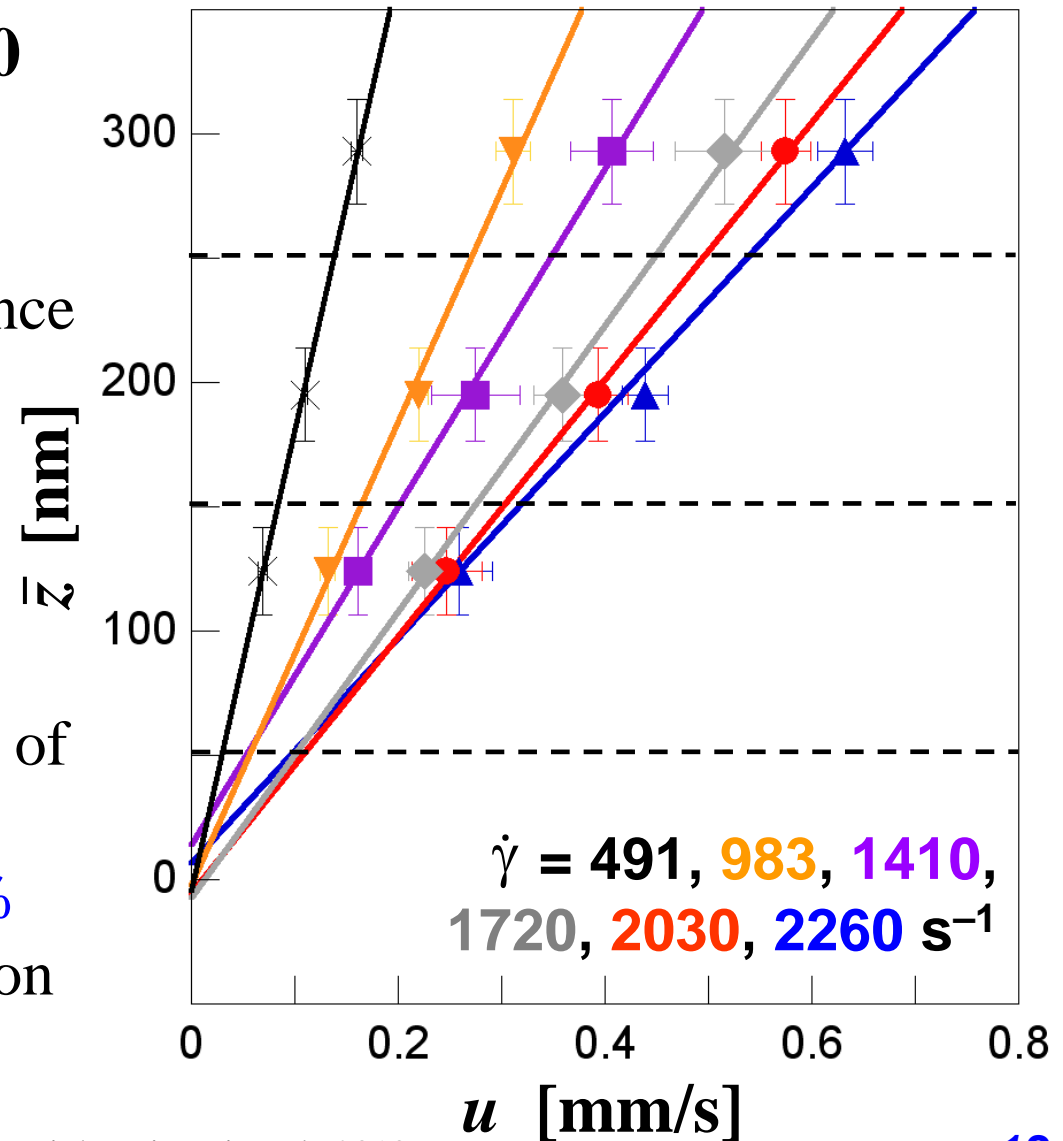
- **Use number density to**

**determine avg.  $z$  for each layer**  $\bar{z}_I = \int_I c(z) z dz / \int_I c(z) dz$

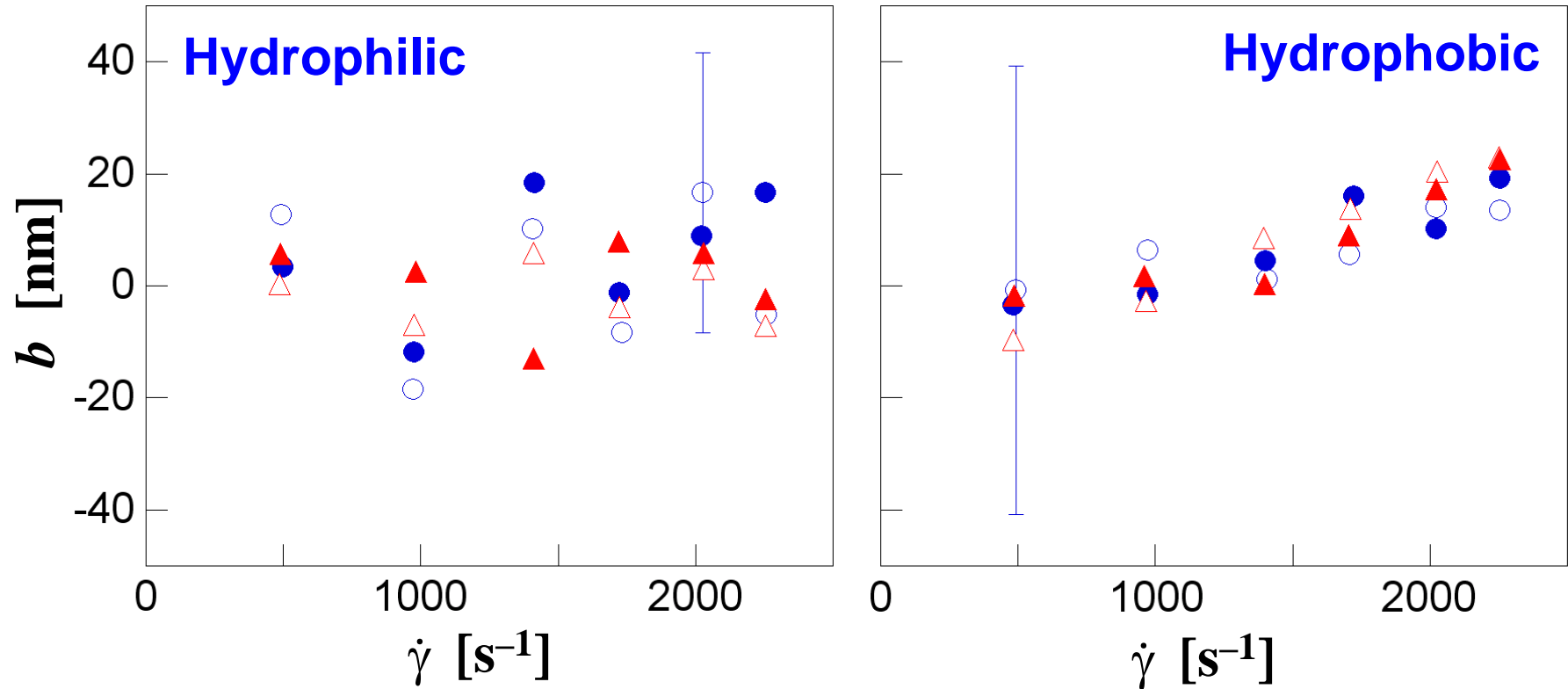


# VELOCITY RESULTS

- **Hydrophilic channel (10 mM, pH7.7)**
  - Average over 5 expts.
  - Error bars 95% confidence intervals
- **Linear curve-fits to data account for uncertainties in  $u$  and  $z$** 
  - Shear rates within 4.5% of exact solution for hydrophilic case and 5% for hydrophobic cases (on average)



# SLIP LENGTHS



- In all but one out of 48 cases,  $b < \text{experimental uncertainty}$ 
  - In that case,  $b = 23 \pm 22$  nm
  - Hydrophobic:  $b$  “more organized”; increases with shear rate

Li & Yoda 10

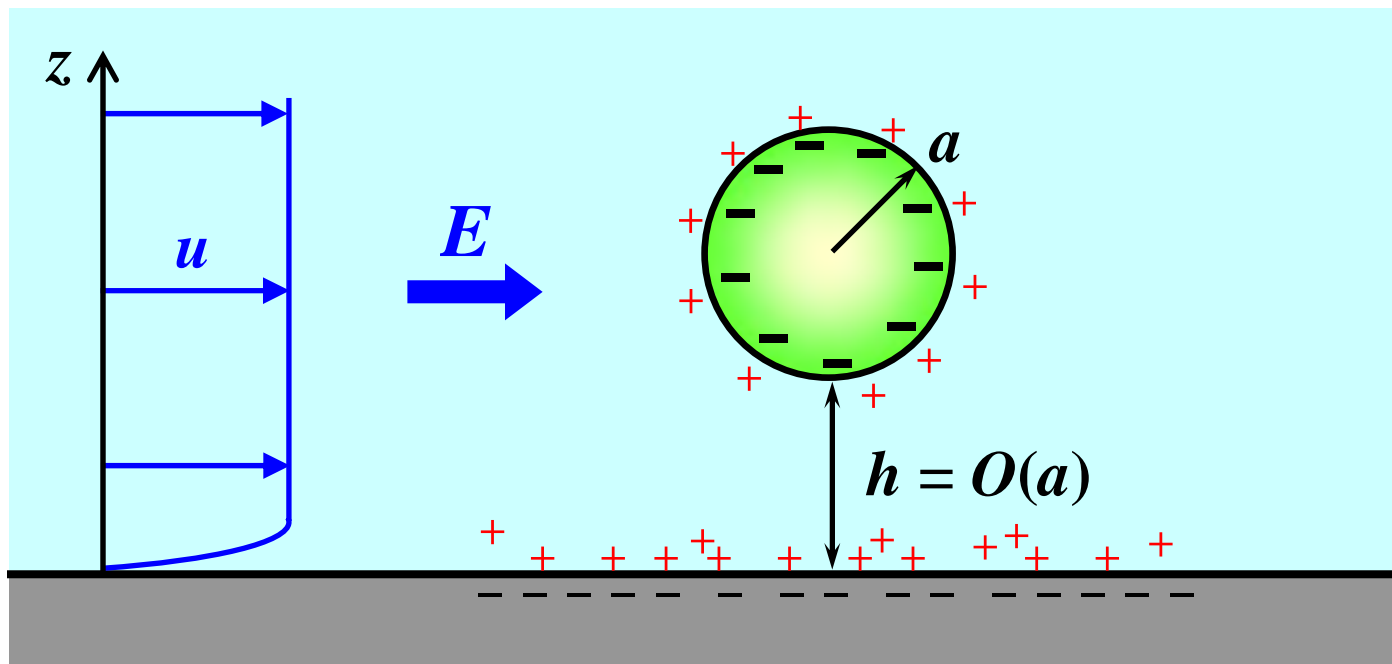


*ELECTROKINETICALLY  
DRIVEN FLOWS*



# A PARTICLE NEAR A WALL

- In addition to Brownian effects, charged particle and wall, conducting fluid with mobile ions
  - For electrokinetically driven flows, external electric field parallel to wall



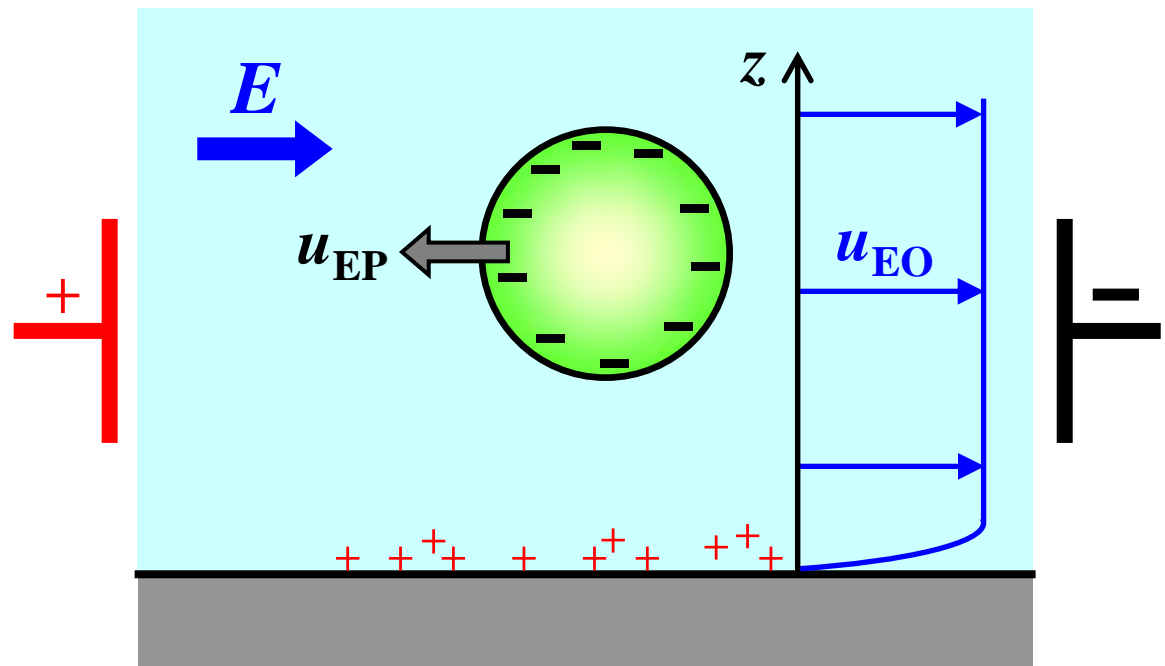


# ELECTROKINETIC EFFECTS

- **Electroosmosis: counterions in wall EDL driven by  $E$** 
  - Fluid away from walls driven by motion of fluid in EDL  $\Rightarrow$  uniform flow outside EDL
- **Electrophoresis: charged particle driven by  $E$**
- **Particle transported by electroosmotic flow, subject to electrophoresis**

- Measured particle speed

$$u_P = u_{EO} - u_{EP}$$



# BROWNIAN DIFFUSION

- Do electrophoretic forces alter near-wall (Brownian) diffusion?

- Balance thermal forces with Stokes drag

- In unbounded fluid, Stokes-Einstein relation  $D_{\infty} = \frac{kT}{6\pi\mu a}$
- Additional hydrodynamic drag due to wall  $\Rightarrow$  anisotropic diffusion parallel, normal to wall
- For diffusion parallel to wall Faxén 22

$$\frac{D_{\parallel}}{D_{\infty}} = 1 - \frac{9}{16}\left(\frac{a}{z}\right) + \frac{1}{8}\left(\frac{a}{z}\right)^3 - \frac{45}{256}\left(\frac{a}{z}\right)^4 - \frac{1}{16}\left(\frac{a}{z}\right)^5$$

- For diffusion normal to wall, approximation of infinite series Brenner 61; Bevan & Prieve 00

$$\frac{D_{\perp}}{D_{\infty}} = \frac{6(z/a)^2 - 10(z/a) + 4}{6(z/a)^2 - 3(z/a) - 1}$$

# EXPERIMENTAL DETAILS

- **Four different fluorescent polystyrene tracers**
  - $a = 110 \pm 12$  nm; particle zeta-potential  $\zeta_p = -60.6 \pm 4.3$  mV
  - $a = 240 \pm 22$  nm;  $\zeta_p = -57.4 \pm 3.1$  mV
  - $a = 371 \pm 34$  nm;  $\zeta_p = -96.2 \pm 2.9$  mV
  - $a = 461 \pm 34$  nm;  $\zeta_p = -99.9 \pm 3.2$  mV
  - Tracers in monovalent electrolyte solution (1 mM, pH~9)  $\Rightarrow$  Debye length scale  $\lambda < 7$  nm
- **Electrokinetically driven flows**
  - $E = 15$  V/cm, 22 V/cm, and 31 V/cm
  - Weak Poiseuille flow ( $E = 0$  V/cm)  $\Rightarrow$  Measured  $u_p < 7$   $\mu\text{m/s}$
- **Image pairs (exp. 0.5 ms) spaced (within pair) by  $\Delta t = 1.3$  ms, 1.6 ms, 1.9 ms and 2.2 ms**

# PARTICLE DISTRIBUTIONS

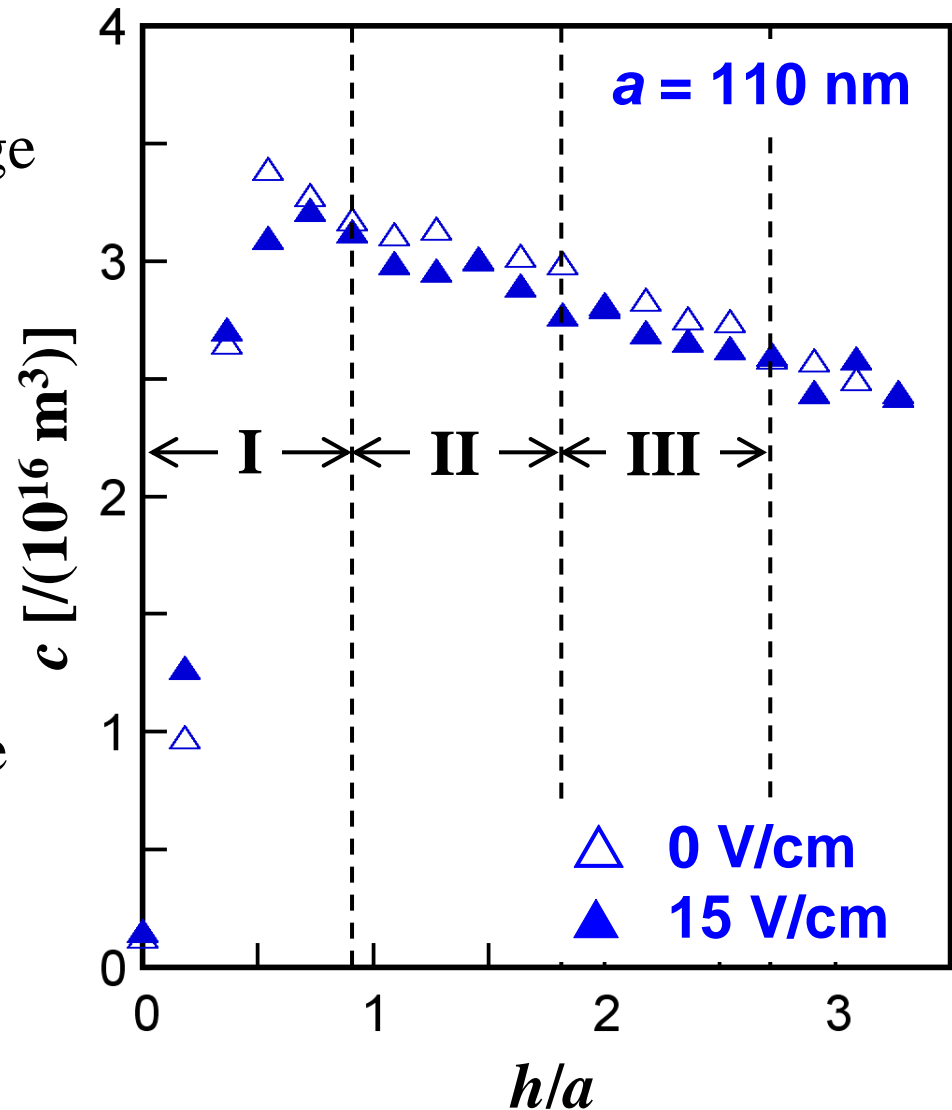
- **Number density  $c$**

- Normalized particle edge distance

$$\frac{h}{a} = \frac{z_p}{a} \ln \left\{ \frac{I_p^0}{I_p} \right\}$$

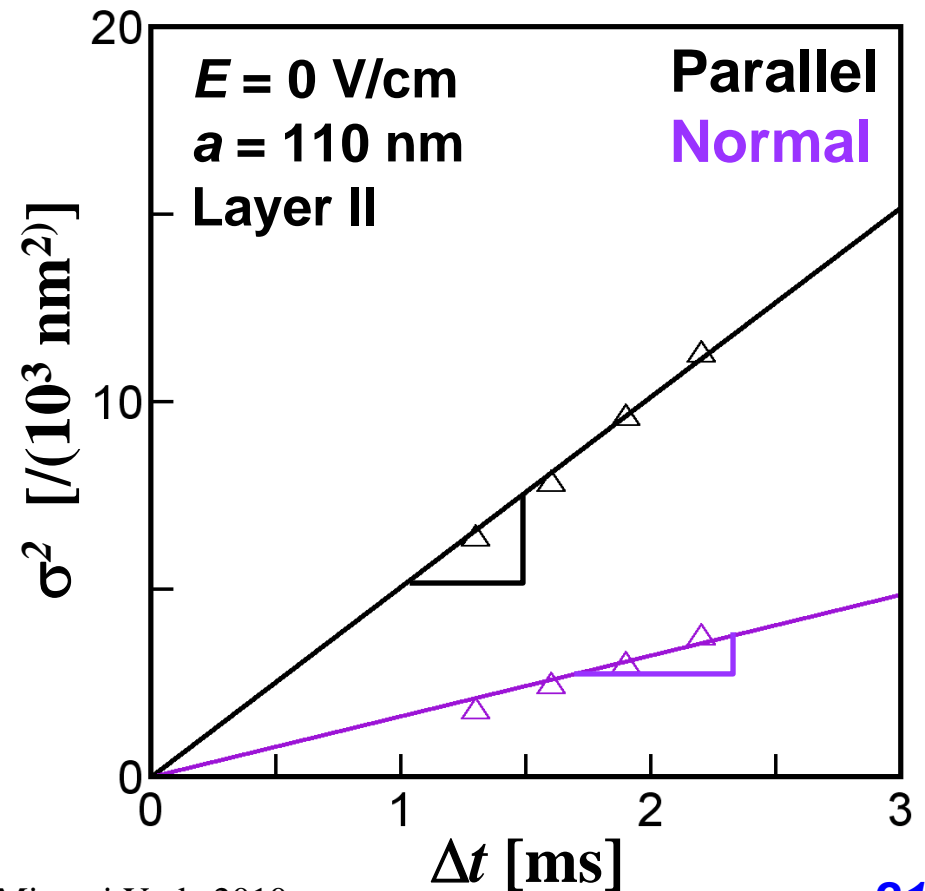
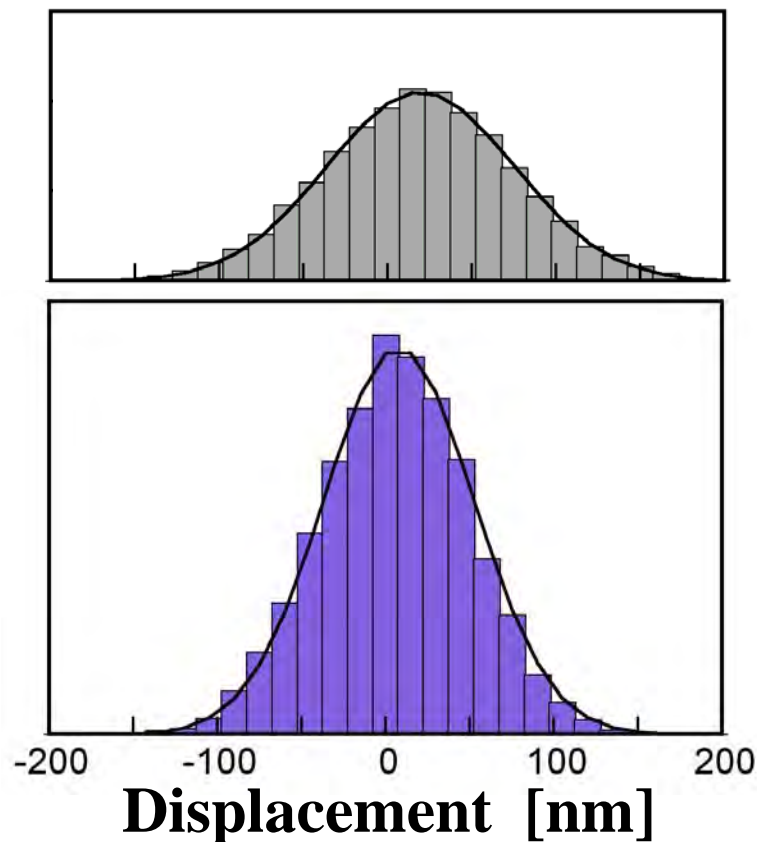
- **Divide  $O(10^5)$  particle images into three (100 nm thick) layers**

- In each layer, determine particle displacements parallel, normal to wall by particle tracking

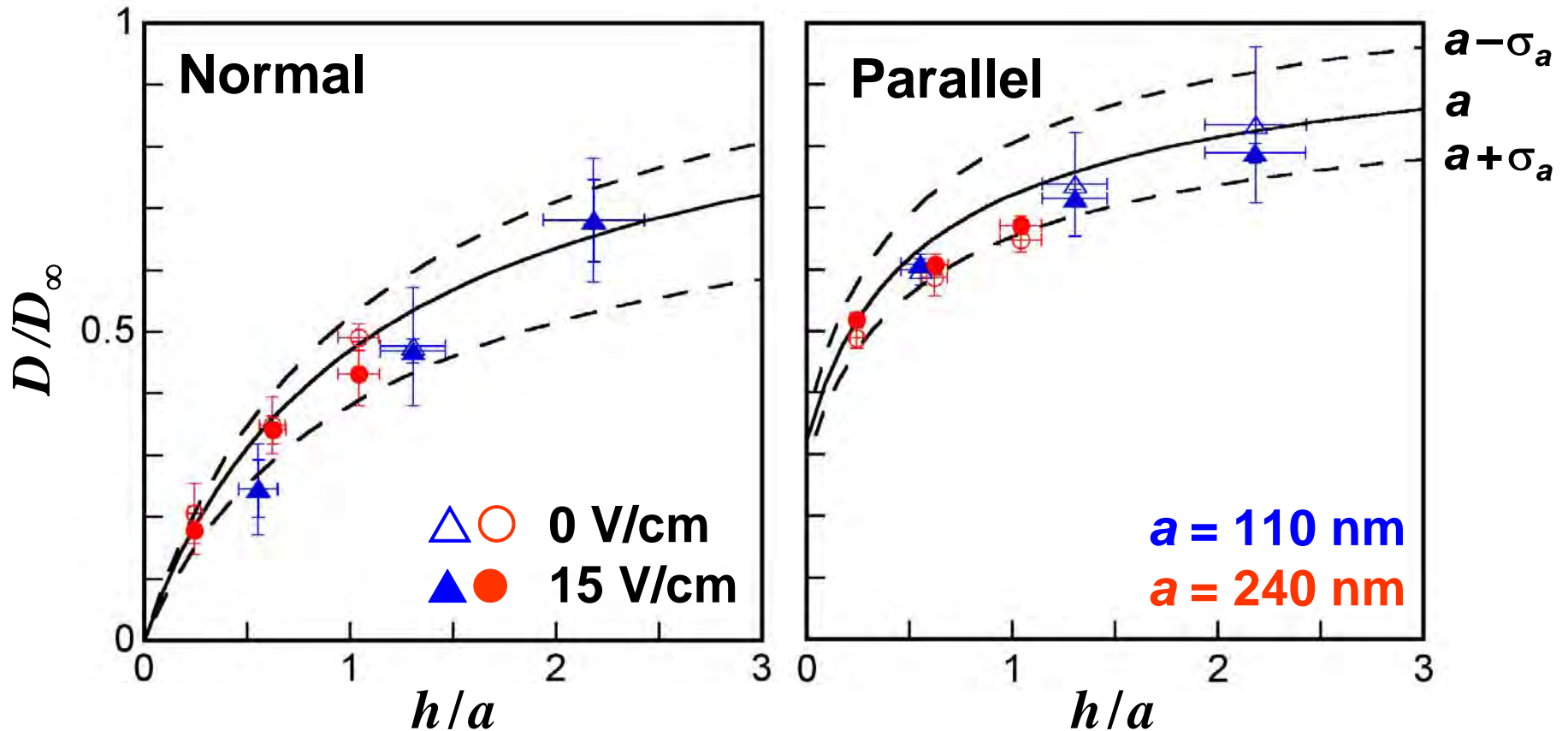


# ESTIMATING DIFFUSION

- PDF of displacements parallel, normal to wall
  - Curve-fit Gaussian: extract  $\sigma^2$  for each layer
- Plot  $\sigma^2$  vs.  $\Delta t \Rightarrow$  slope =  $4D_{\parallel}(\Delta t)$ ,  $2D_{\perp}(\Delta t)$



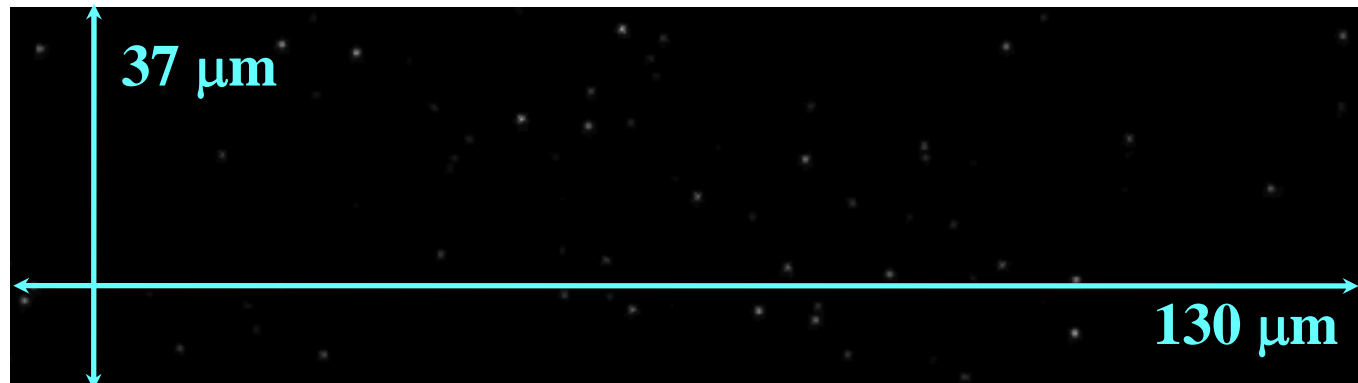
# DIFFUSION RESULTS



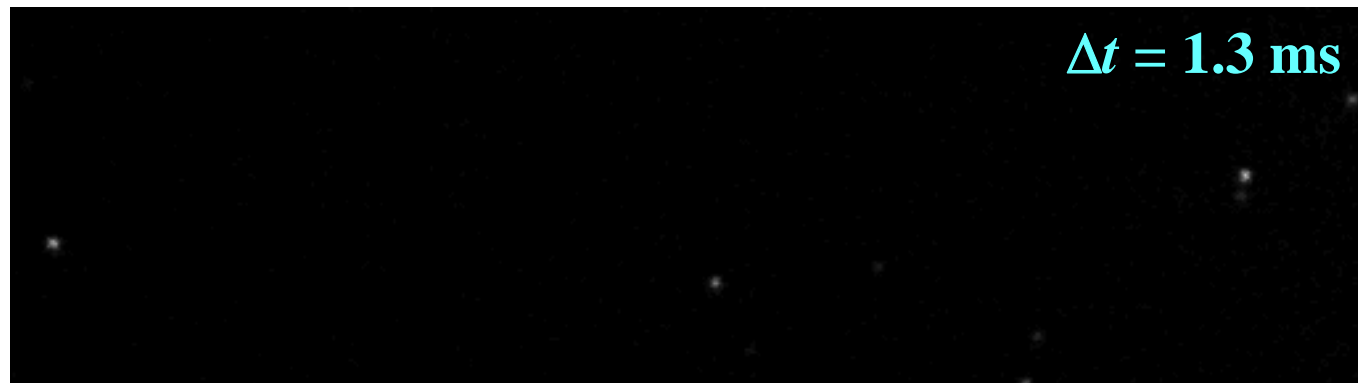
- Data at  $E = 0$  V/cm, 15 V/cm agree and agree with theory
  - $h$ -positions of  $D_{\parallel}$ ,  $D_{\perp}$  determined from particle distributions  $c(h)$
- No discernible effect of external electric field on diffusion

# FLOW VISUALIZATION

$a = 110 \text{ nm}$

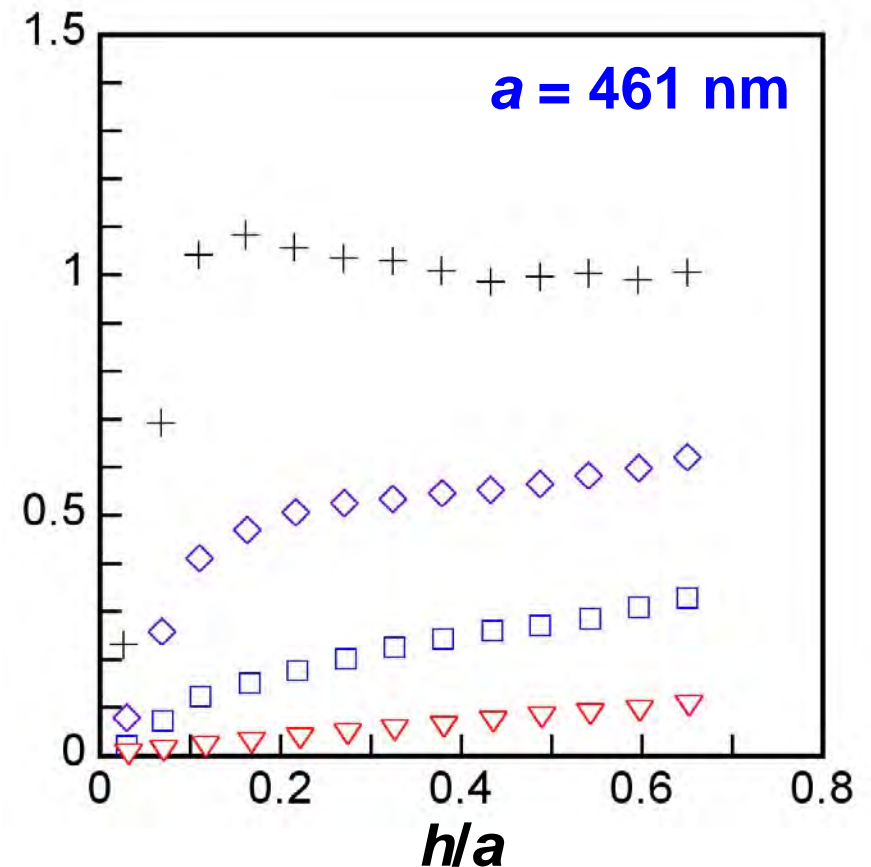
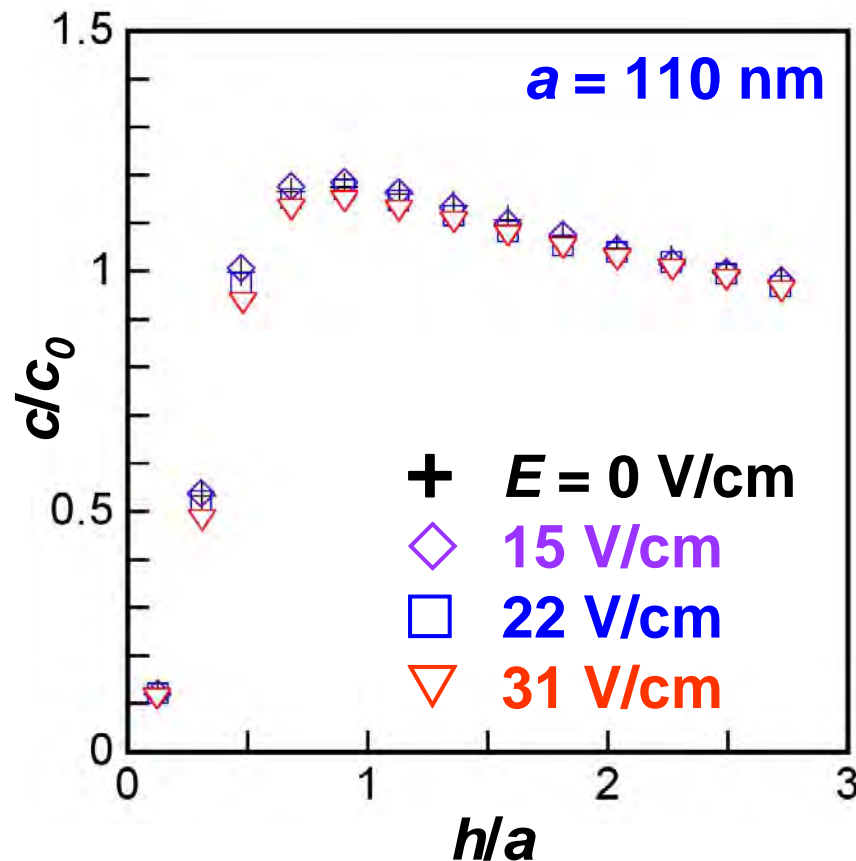


$a = 461 \text{ nm}$



- **Electrokinetically driven flow:  $E = 0 \text{ V/cm}$ , then  $31 \text{ V/cm}$** 
  - $E$  drives larger particles farther away from wall

# PARTICLE DISTRIBUTIONS



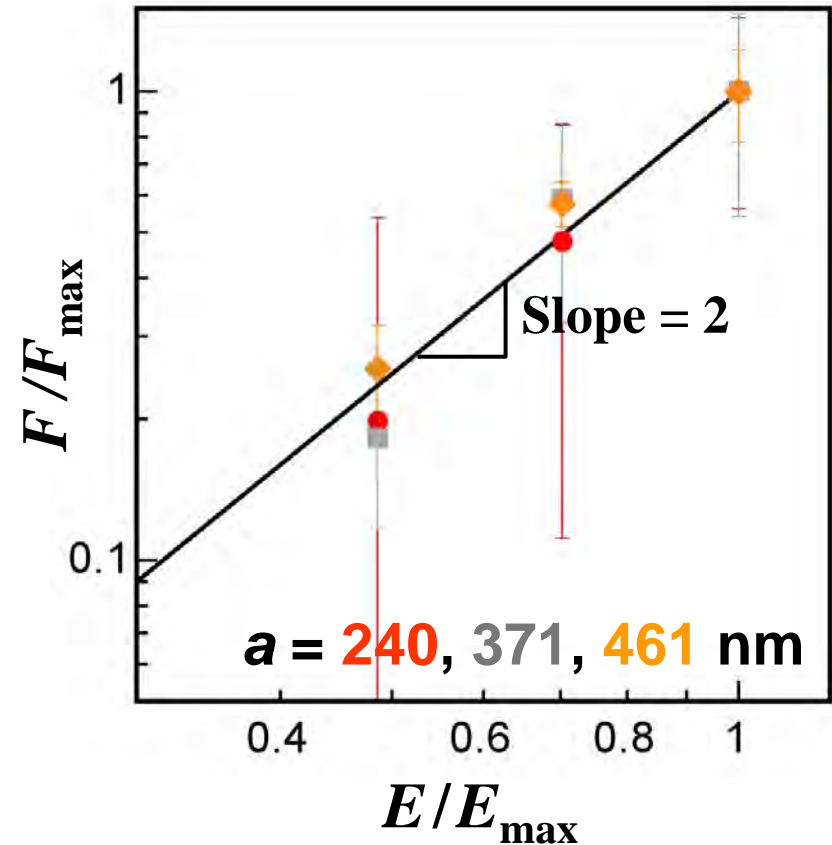
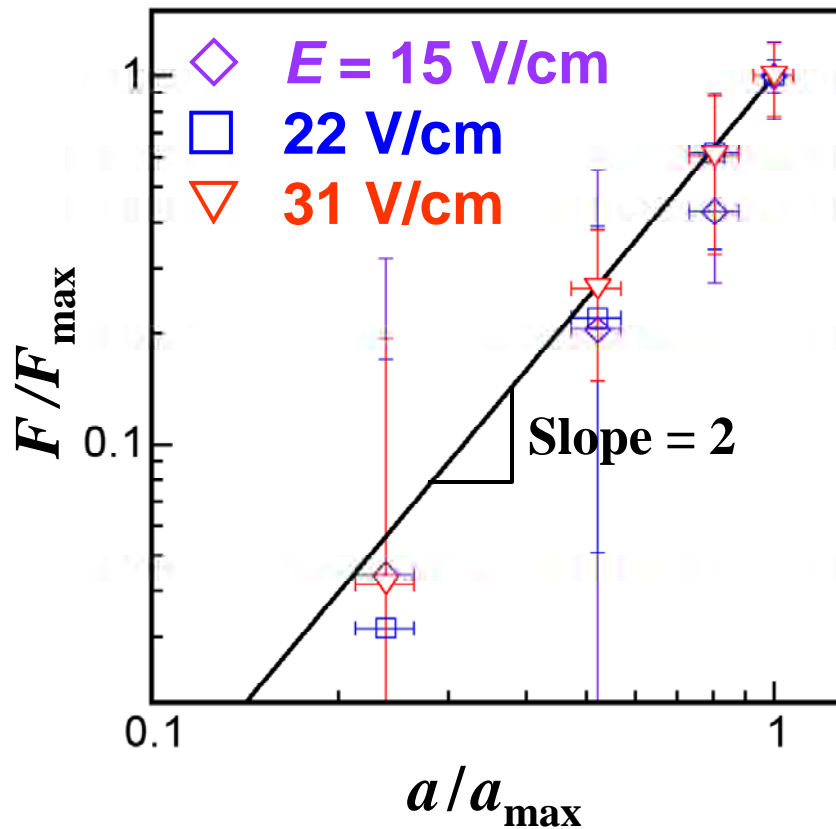
## ■ “Electrokinetic lift”

- Dielectrophoretic-like force due to nonuniform electric field in particle-wall gap

Yariv 06



# "LIFT" FORCE



## ■ Estimate lift force assuming Boltzmann distribution

- Force on particle  $F \propto a^2, E^2$ : no discernible effect of  $\zeta_p$
- $F = O(10^{-14}$  N) for  $E = O(10$  V/cm)

# SUMMARY

- **Evanescent wave-based particle tracking**
  - Measure particle displacements and steady-state particle distributions within  $O(100 \text{ nm})$  of wall
- **Poiseuille flow**
  - Slip lengths of Newtonian liquids over hydrophilic and hydrophobic surfaces zero within experimental uncertainties after accounting for nonuniform tracer distributions
- **Electrokinetically driven flow ( $E$  parallel to wall)**
  - Moderate electric fields appear to have no effect on diffusion
  - Using H-S to predict electrophoretic velocity, even within  $O(a)$  of wall gives good estimate of electroosmotic flow
  - Dielectrophoretic-like force  $\Rightarrow$  particles farther from wall: force scales as  $a^2, E^2$

# ACKNOWLEDGEMENTS

- **Haifeng Li: Poiseuille flow**
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